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(54) Title: OXIDIZED CELLULOSE-CONTAINING FIBROUS MATERIALS AND PRODUCTS MADE THEREFROM			
(57) Abstract			
<p>The present invention relates to a cellulose-containing fibrous material, wherein hydroxy groups were oxidized at the C(6) of glucose units of the cellulose into aldehyde and/or carboxy groups, a paper or nonwoven (product) made therefrom, in particular tissue (products) and a process for their manufacture. The paper or nonwoven (products) of the invention display excellent strength properties.</p>			

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the one hand and the textile products on the other and are nowadays summarized under the term "nonwovens" (see ISO 9092 - EN 29092). As regards the production of nonwovens, a large number of extremely varied production processes is used, such as the so-called air-laid and spun-laid techniques, as well as so-called wet-laid techniques, the former as a typical choice from the so-called dry-laid techniques predominating by far and the wet-laid techniques similar to paper manufacturing forming more a marginal group.

Today, the nonwovens are understood as an independent group of products. Nonwovens include mats, nonwoven fabrics and finished products made therefrom, in many cases for hygiene requirements. These composite materials, which frequently resemble textiles, represent flexible porous fabrics that are not produced by the classic methods of weaving warp and weft or by looping, but by intertwining and/or by cohesive and/or adhesive bonding of typical synthetic textile fibers which may for example be present in the form of endless threads or threads prefabricated with an endless length, as synthetic threads produced *in situ* or in the form of staple fibers. Alternatively, they may be made of blends of synthetic fibers in the form of staple fibers and natural fibers, e.g. natural vegetable fibers (see DIN 61 210 T2 of October 1988 and ISO 9092 - EN 29092).

"Papers" are also planar materials, albeit essentially composed of fibers of a vegetable origin and formed by drainage of a fibrous-material suspension on a screen or between two endless revolving screens and by subsequent compression and drainage or drying of the thus produced mat (cf. DIN 6730, May 1996). The standard restricts the range of mass per unit area (basis weight) for paper to less than / equal to 225 g/m<sup>2</sup>.

In German standard DIN 6730, the German term "Karton" (= cardboard) has a definition similar to paper, though the

basis weight range extends from 150 g/m<sup>2</sup> to 600 g/m<sup>2</sup>, i.e. there is an overlap here with respect to paper. The term *Karton* is common only in German-speaking countries.

The German term "*Pappe*" (= (paper)board) is defined in DIN 6730 as a generic term for solid board and corrugated fibre board and encompasses products in the basis weight range above 225 g/m<sup>2</sup>.

Based on the underlying compatibility of the production processes (wet laying), "tissue" production is counted among the paper making techniques. The production of tissue, or more accurately, raw tissue if the one-ply (intermediate) product manufactured on a special-purpose paper machine of the tissue or tissue paper machine is meant, is delimited from paper production as a result of the extremely low basis weight of normally less than 65, more often less than 40 g/m<sup>2</sup> and as a result of the much higher tensile energy absorption index. The tensile energy absorption index is arrived at from the tensile energy absorption in which the tensile energy absorption is related to the test sample volume before inspection (length, width, thickness of sample between the clamps before tensile load). Paper and tissue paper also differ in general, as do tissue papers which differ from the raw material, chemical additives and production conditions with regard to the modulus of elasticity that characterizes the stress-strain properties of these planar products as a material parameter.

A tissue's high tensile energy absorption index results from the outer or "inner" creping. The former is produced by compression of the paper web adhering to a drying cylinder as a result of the action of a crepe doctor or in the latter instance as a result of a difference in speed between two fabrics. In the latter technique, often referred to as "(wet) rush transfer", for instance the forming fabric of the paper machine is moved at greater speed than the fabric the formed

paper web is transferred to, for instance a transfer fabric or a TAD fabric (through air drying), so that the paper web is bundled somewhat when it is taken up by the transfer fabric. This causes the still moist, plastically deformable paper web to be internally broken up by compression and shearing, thereby rendering it more stretchable under load than paper which has not been subjected to outer or inner creping. Many prior art documents (e.g. EP-A-0 617 164, WO-94/28244, US-5 607 551, EP-A-0 677 612, WO-96/09435) mean this "inner creping", if they describe the production of "uncreped" tissue paper by rush transfer techniques.

Most of the functional properties typical of tissue and tissue products result from the high tensile energy absorption (see DIN EN 12625-4 and DIN EN 12625-5).

An example of papers and paper products is represented by hygiene papers, particularly tissue papers and hygiene products (tissue products) made therefrom and which are e.g. used in personal grooming and hygiene, the household sector, industry, the institutional field in a wide variety of cleaning processes. They are used to absorb fluids, for decorative purposes, for packaging or even as supporting material, as is common for example in medical practices or in hospitals. In terms of their wide variety, hygiene products are now considered to be everyday products.

Hygiene paper primarily includes all kinds of dry-creped tissue paper, as well as wet-creped paper and cellulose or pulp wadding.

The one-ply intermediate products originating from the paper machine and made of lightweight paper usually dry-creped on a yankee cylinder by means of a crepe doctor are generally described as "tissue paper" or more accurately raw tissue paper. The one-ply raw tissue may be built up of one or a plurality of layers respectively.

All one-ply or multi-ply final products made of raw tissue and tailored to the end user's needs, i.e. fabricated with a wide variety of requirements in mind, are known as "tissue products".

Typical properties of tissue paper include the ready ability to absorb tensile stress energy, their drapability, good textile-like flexibility, properties which are frequently referred to as bulk softness, a high surface softness, a high specific volume with a perceptible thickness, as high a liquid absorbency as possible and, depending on the application, a suitable wet and dry strength as well as an interesting visual appearance of the outer product surface. These properties allow tissue paper to be used for example as cleaning wipes, sanitary products (e.g. toilet paper), paper handkerchiefs, cosmetic wipes (facials) or as serviettes/napkins.

The invention's range of applications nevertheless also includes those materials or products which are known as "fluff" products in specialist circles, such as absorptive material for diapers/nappies, articles of feminine hygiene including sanitary napkins/towels, tampons, slips or incontinence articles for adults, and the like..

Papers and paper products are often exposed to extremely varied strength requirements in the wet and dry states. For instance, it must be ensured in the case of packaging paper that it also retains its strength at least for a specific period of time when exposed to rainwater. On the other hand, toilet paper should dissolve in water - some time after use - in order to prevent the sewage systems from clogging up. At the same time, toilet paper must not immediately lose its strength properties during use, i.e. whenever it has just briefly come into contact with the moisture from excrement.

To describe the strength properties of paper, the prior art therefore often draws a distinction between a paper's "dry strength", "initial wet strength", "temporary" and "permanent" wet strength. This also applies to tissue paper and tissue products.

Dry strength is generally determined in a similar manner, in the case of paper usually based on DIN EN ISO 1924-2, Paper and Board, Determination of properties under tensile load. Part 2: method at a constant rate of elongation, April 1995, (ISO 1924-2 : 1994). In the case of tissue paper and tissue products, tests are performed on the basis of DIN EN 12625 - 4, Tissue Paper and Tissue Products - Part 4: determination of width-related breaking strength, elongation at break and the tensile energy absorption, January 1999.

The term "initial wet strength" was originally used just to characterize half-stuffs for paper production such as groundwood pulp, but was later extended to chemical pulp. The initial wet strength is calculated on a 100 g/m<sup>2</sup> test strip produced on the Rapid Köthen device in accordance with German Zellcheming Code of Practice VI/6.

Similarly, the initial wet tensile strength index, initial wet tensile stretch behavior and initial wet-strength energy absorption index of a wet-pressed laboratory sheet are calculated in accordance with SCAN M 11 and SCAN M 12, with the difference that in these instances, the test strips of the obtained laboratory sheets are tested according to the normal methods of strength testing by means of an electronic tensile testing machine, without needing special-purpose testing equipment (see Werner Franke (editor), *Prüfung von Papier, Pappe, Zellstoff und Holzstoff*, Vol. 3, *Physikalisch-technologische Prüfung der Papierfaserstoffe*, pp. 86-87, Springer-Verlag, ISBN 3-540-55896-9).

The initial wet strength originally characterized the strength after sheet formation, and particularly refers to the strength of the initially formed moist paper web at the time of the first free transfer e.g. from the screen section to a subsequent press section.

More recent prior art defines initial wet strength more broadly than earlier prior art. This definition essentially acts as a parameter for characterizing the strength behavior of remoistened paper, paper products, tissue paper and tissue products. It is ascertained as the tensile strength of paper soaked over a specific period of time.

In this way, WO 97/36052 and US 5,760,212 do indeed define the initial wet strength by means of the normal wet strength determination employed in comparable measuring techniques. Yet the so-called initial wet strength here corresponds to the wet strength of a sample (test strip) from a test sheet exhibiting a predetermined basis weight and produced under standardized conditions, calculated - after previously soaking the test strip - using a standardized tensile testing device under standardized test conditions.

In addition to the initial wet strength, the aforementioned documents introduce and use the terms "temporary" and "permanent" wet strength as further criteria for evaluating the strength of a product after it has been remoistened (wet strength) and hence as criteria for its suitability in everyday practice (for example the dissolving properties of toilet paper after it has been used in order to avoid clogging up the pipes). The soaking duration and decrease in wet strength over time are used in these documents as criteria to differentiate between initial, temporary and permanent wet strength.

In these documents, a rate of decrease is mathematically determined on the basis of measured values as a criterion for



the evaluation of temporary wet strength in that the difference is formed from the so-called initial wet strength as the wet strength after 5 s soaking duration and the wet strength after 30 min soaking duration for samples that were somehow pretreated e.g. by addition of a wet-strength agent or by modification of the fibrous material in order to increase wet strength. The difference of the corresponding measurements for untreated samples is calculated in a similar way. The difference of the strengths of the treated samples is then placed in proportion to the difference of the strengths of the untreated samples and expressed as a percentage.

In simplified terms, this means that temporary wet strength should be defined as the drop in strength of a sheet of paper or tissue paper or of a tissue product; after remoistening the paper, tissue paper or tissue product after expiry of an interval of the action of moisture (soaking) to be specified by definition, this drop can be determined in terms of measurement technology by means of a standard test method. In contrast, the permanent wet strength should be defined as the maintenance of strength even after moisture has exerted its influence for a fairly long time upon remoistening e.g. for a period of 30 min.

The same applies to nonwovens and products made thereof.

When experimentally checking the present invention, a similar approach was adopted in principle, though existing national, European or international standards were as far as possible fallen back on in the calculation and description of the results, and the comparisons between treated and untreated samples were made only on the basis of a (wet) tensile strength also designated as initial wet strength.

Additional definitions for suitable parameters, e.g. a broader definition of initial wet strength, are derived from the above in order to describe the results regarding an increase in

additives, modified soluble cellulose derivatives are used as wet-strength agents. In this way, for example, the addition of carboxymethyl cellulose is usual as an additive besides the aforementioned polyamide epichlorohydrin resins.

To bond cellulose fibers together according to the second technique, thereby increasing the strength, US-5 873 979 teaches the reaction of the cellulose's hydroxy functions with a C2-C9 dicarboxylic acid.

Modified techniques for increasing the strength of paper in the wet state are taught in the following applications filed by the Procter & Gamble Company: WO 97/36051, WO 97/36053, WO 97/36037, WO 97/36054 and WO 97/36052.

WO 97/36051 describes paper that exhibits a temporary wet strength and which is obtained by linking a polyhydroxy polymer (e.g. cellulose) to 1,2-disubstituted alkene carboxylic acid, oxidative cleavage of the double bond of the alkene carboxylic acid into aldehyde functions and crosslinking the hydroxy groups of the polyhydroxy polymer with the aldehyde functions.

WO 97/36053 describes a paper product exhibiting temporary wet strength and comprising (a) cellulosic fibers and (b) a binder which has (b-i) a polyaldehyde polymer and (b-ii) a water-soluble polysaccharide with cis-OH groups.

WO 97/36037 describes the aldehyde-modified cellulosic fibers upon which the paper product according to WO 97/36051 is based.

WO 97/36054 discloses a compound that bestows temporary wet strength on paper products and which comprises the ozone oxidation product (containing aldehyde groups) of a polysaccharide in which the OH groups in at least one recurrent unit of the polysaccharide are OH groups in cis

position. This document also describes a paper product that comprises cellulosic fibers in combination with the above compound and a method of producing the compounds of the paper product.

WO 97/36052 describes a paper product exhibiting initial wet strength and comprising

- (a) cellulosic fibers having free aldehyde groups originating from cellulosic fibers that include a polysaccharide (preferably galactose and/or mannose) in which the OH groups of least a part of the recurrent units are OH groups in cis position, in combination with
- (b) a water-soluble polymer having functional groups that can react with the aldehyde groups.

Since cellulose exhibits OH groups in trans position, the hemicellulose portion of pulps that have a high proportion of hemicellulose is to be oxidized and the oxidation product used as a "binder". Hemicelluloses are derived from (poly)saccharides with OH groups in cis position (e.g. galactose, mannose) that can be rapidly oxidized into aldehyde groups and which can then form (hemi)acetal bonds in accordance with the teaching of this document, such bonds holding the paper product together.

The present invention's object is therefore

- to make available a cellulose-containing fibrous material that can also result in paper/nonwoven (products) without use of additives and exhibiting suitable strength parameters;
- and to make available the production processes for this fibrous material, paper/nonwovens and paper/tissue paper/nonwoven products.

This object is solved by a cellulose-containing fibrous material in which OH functions at the C(6) of the glucose unit of the cellulose are oxidized into aldehyde and/or carboxyl groups. The content of aldehyde groups particularly influences wet strength, whereas carboxyl groups particularly contribute toward enhancing dry strength.

The present invention also relates to a paper/tissue paper/nonwoven, whereby within the framework of the present invention, the tissue paper forms a particularly preferred embodiment of the paper that contains this fibrous material; the invention likewise relates to a paper/nonwoven product, particularly a tissue product, composed of at least one ply of paper/nonwoven according to the invention. Each ply may comprise one or more layers that include the fibrous material according to the invention.

Lastly, the present invention's subject matter is also constituted by methods of producing the fibrous material, paper/nonwoven and the paper/nonwoven product.

#### OXIDIZED CELLULOSE-CONTAINING FIBROUS MATERIAL

The fibrous material according to the invention contains cellulose in which OH functions at the C(6) of the glucose unit are oxidized into aldehyde and/or carboxyl groups. In accordance with the invention, however, the presence of other oxidized groups in the fibrous material is not ruled out.

Cellulose is defined here as the long-chain fibrous portion insoluble in 10% (wt.%) NaOH ( $R_{10}$  portion) and which is also known in older literature as  $\alpha$ -cellulose (to determine the  $R_{10}$  value see ASTM Method D1695, Annual Book of ASTM standards, Section 15, Vol. 15.04, American Society for Testing and Materials, Philadelphia 1983 and "Cellulose Chemistry and its Applications", edited by T.P.Nevell and S.H. Zeronian, Ellis Harwood Pub., West Sussex, England 1985, p.16 et seq.).

The cellulose portion ( $R_{10}$  value) is preferably at least 50%, particularly at least 85%, relative to the total weight of the oven-dried fibrous material (The term "oven-dried" refers to the determination of the dry content of fibrous material/pulp samples corresponding to DIN EN 20638). Greater preference is given to values of at least 90%, particularly of at least 95%.

Cellulose is present in the cells, particularly of lignified plants, in a proportion of up to 50% of the mass, whereas hemicelluloses and lignin account for the remaining 50% of the mass of lignified plant, depending on the particular variety in varyingly large proportions (see Dietrich Fengel and Gerd Wegener, Chemistry, Wood, Ultrastructure, Reactions, Walter de Gruyter (1984)).

The pulps that can be used according to the invention for the purpose of oxidation are not subject to any specific restrictions regarding the degree of polymerization (DP) of the glucose molecules in the cellulose, the wall layer of plant cell from which the cellulose originates, the type of plant cell from which the cellulose originates etc., there being differences specific to the origin in each case. Since the structure of the plant cell wall is inhomogeneous and this inhomogeneity exhibits distinct features of layering (texture), individual cell wall layers can be clearly distinguished from one another. A distinction can also be made with regard to the type of plant cell. In addition to tracheids or fibrous tracheids, vascular cells or libriform fibers or parenchymatous cells, inter alia, thus occur in cellulosic fibrous materials. There are also considerable differences regarding the layering in the various plant cells.

The cellulose in the cellulose-containing fibrous material preferably has a number-averaged molecular weight of 3000 to 1 million g/mol, particularly 3000 to 10,000 g/mol.

The cross section of the plant cells that form the fibrous material according to the invention, and the ratio of the wall to lumen may fluctuate within broad limits due to the plant's morphology. This is caused by the fact that it is possible to distinguish between different cells within a plant (see Dietrich Fengel and Gerd Wegener; Wood, Walter de Gruyter (1984), p. 12, Table 2-2).

In the case of gymnosperms and most of the angiosperms, this is caused by the formation of spring wood and late wood and the formation of reaction wood. The formation of reaction wood occurs on the pressure side in the case of angiosperms, whereas it is formed on the tensile side in the case of gymnosperms. It is typical that in the case of reaction wood, the ratio of wood to lumen compared to other plant cells is much larger, i.e. the remaining lumen diameter of these cells is much smaller.

In addition, as mentioned above, it is possible to differentiate within the wall of the plant cell with regard to layering. Upon considerable magnification, this layering can be represented even in visible light (see Dietrich Fengel and Gerd Wegener; Wood, Walter de Gruyter (1984), p. 13, Fig. 2-12 b; p. 15, Fig. 2-14).

An essential feature of the invention is that the cellulose itself, and not just accompanying portions of the cellulose-containing fibrous material (e.g. hemicellulose in pulp), exhibits aldehyde and/or carboxyl groups.

It has been found that the fibrous material according to the invention may lead to paper/nonwoven (products) with excellent strength properties, particularly a high wet strength and a high relative wet strength.

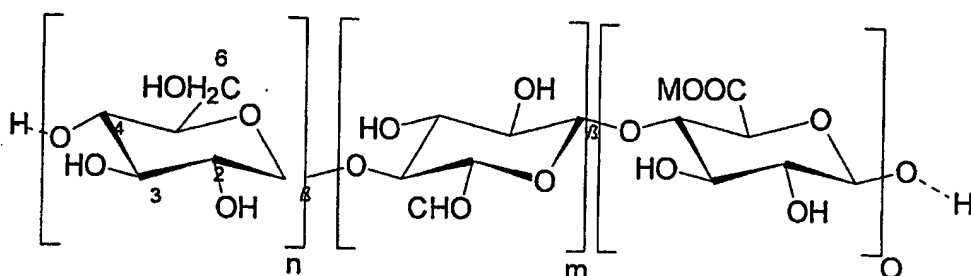
A model that explains the observed increase in strength, particularly the increase in wet strength, is based on the formation of (hemi)acetal bonds between aldehydes and the OH groups of the cellulose chain molecules from the accessible outer wall surfaces of adjacent fibers when these cellulose

chain molecules of adjacent fibers come so close together in the inter-fiber gap at least over a partial portion of its length that the aforementioned bonds are produced. The dry strength, on the other hand, is above all based on the formation of hydrogen bridges between the carboxy/aldehyde groups and the remaining HO groups of the cellulose. The invention is not, however, restricted to this hypothesis.

The strengths achievable just using an oxidized cellulosic fibrous material according to the invention in the planar intermediate product (paper, particularly tissue paper) or in the planar end product (paper product, particularly tissue product), particularly wet strength, are significantly higher than those when just using the same fibrous material, particularly pulp, that has not, however, been modified by oxidation, when it is assumed that no additional measures such as beating and/or addition of chemical auxiliary substances like wet-strength agents occur.

In particular, the wet strengths of such papers, particularly tissue papers and end products made therefrom, are at least 10 times greater than the wet strengths of papers, particularly tissue papers, made of comparable fibrous raw materials not modified by oxidation; further preference is for these strengths to be at least 20 times greater, even further preference is for them to be at least 30 times greater, and most preference is for them to be at least 40 times greater.

The fibrous material according to the invention is characterized by aldehyde and/or carboxyl groups on the C(6) of the glucose unit of the cellulose. Preferably the glucose units that carry the C(6)-aldehyde and/or carboxy groups are largely intact. A cellulose chain solely oxidized at C(6) is described by the following formula:



where the above units may be statistically distributed over the chain, M is hydrogen or a cation, and n, m and o may be 0 or an integer  $\geq 1$ , on condition that m and/or o is not 0.

The total content of aldehyde and/or carboxyl groups at C(6) is preferably more than 50 or more than 100  $\mu\text{mol/g}$  dry weight (oven-dried) of the fibrous material, particularly more than 150  $\mu\text{mol/g}$ . Even greater preference is given to values of more than 200  $\mu\text{mol/g}$ , particularly more than 250  $\mu\text{mol/g}$ . If the C(6)-atoms of the cellulosic glucose units carry a mixture of aldehyde and carboxy groups, the content of C(6)-aldehyde groups thus preferably also is more than 50, 100, 150, 200 or 250  $\mu\text{mol/g}$  with increasing preference in this order. In the claimed cellulose-containing material, the cellulose preferably contains at least 1 C(6)-aldehyde groups per 100, especially per 50 or even 25, monosaccharide (glucose) units. whereby a possible (hemiacetalised) aldehyde group at the reducing end of the cellulose chain does not count. Preferably the number of aldehyde groups is greater, especially more than two times greater than the number of carboxyl groups.

The content of oxidized groups in the fibrous material according to the invention can be analytically determined as explained in the section "examples".



## PAPER/TISSUE PAPER/NONWOVEN ACCORDING TO THE INVENTION

The introduction of the description is referred to for the definition of the terms "paper", "tissue paper" and "nonwoven". It should be mentioned that the term "tissue" includes material with outer and/or inner creping, the latter being obtainable by (wet) rush transfer techniques.

The paper/tissue paper/nonwoven according to the invention comprises the fibrous material according to the invention. Other fibers can optionally be added in quantities of preferably up to 95 wt.%, more preferably up to 70wt.% .%, even more preferably up to 50wt.%, relative to the total weight (oven-dried) of the paper/tissue paper/nonwoven.

Even if it is possible according to the invention to achieve an increase in strength without wet-strength agents, the addition of wet-strength agents may be appropriate in individual cases in order to achieve a further improvement in strength properties (preferred maximum content: 20% wt.%, relative to the total weight of the oven-dried paper/tissue paper/nonwoven). Examples of suitable wet-strength agents are: carboxymethylcellulose, PAE (polyamine-amido-epichlorohydrin resin), polyacrylamide, urea formaldehyde resins and prepolymers thereof, melamine formaldehyde resins and prepolymers thereof as well as phenol formaldehyde resins and prepolymers thereof.

The paper/tissue paper/nonwoven according to the invention is preferably a hygiene paper, particularly a tissue paper. It preferably has a basis weight of up to 225 g/m<sup>2</sup>. In the case of a (one-ply) tissue paper, the basis weight is usually at least 8 g/m<sup>2</sup>, preferably 10 to 60 g/m<sup>2</sup>, with greater preference on 13 to 40 g/m<sup>2</sup>, particularly 15 to 30 g/m<sup>2</sup>.

The term "paper/nonwoven", e.g. "tissue paper", is used here for planar products having a ply composed of at least one

layer, this ply having a portion of preferably at least 10% fibrous material according to the invention, with further preference for at least 20%, further preference for at least 30%, even further preference for at least 50%, and most preference for at least 70% of this fibrous material. The ply may, however, comprise a plurality of layers, preferably 1 - 10 layers, depending on the production process. (The term "paper/tissue paper/nonwoven product" explained in the following section is used for planar (end) products having one or more plies. Each ply comprises at least one layer; each layer may differ in terms of its material composition). The term "layers" refers to a change in physical and/or chemical properties perpendicular to the layer plane, caused e.g. by the use of different fibrous raw materials per layer, as is possible by systematic fiber feed at the headbox of the paper machine. Headboxes of paper or tissue machines usually have one-, two- or three-layer headboxes, thus enabling very systematic layering within the ply, which leads to an improvement in the mechanical properties. The fibers are bonded together within the layer and between the layers by hydrogen bridges and/or covalent bonds and/or other conceivable chemical and physical forces such that nondestructive separation of the layers is no longer possible or possible only with difficulty. The term "ply" on the other hand describes the planar fibrous material product comprising one or more layers, as usually obtained on the paper machine, particularly the tissue paper machine, or as obtained as a continuous web during nonwoven production. In the case of a planar fibrous material product that comprises a plurality of plies, these plies are usually brought together after drying the web. The term "plies" is therefore used if separation is easily possible (for example most of the multi-ply paper handkerchiefs can be separated into the individual plies as a result of pulling them apart).

The paper/nonwoven (particularly tissue paper) according to the invention exhibits the following strength parameters which each refer to measurements on a "ply".

For those reasons explained at the start, the wet tear length of the paper/tissue paper/nonwoven according to the invention is less than the dry tear length. The wet tear length is preferably more than 200 m, particularly more than 400 m or more than 500 m. Even greater preference is given to values of more than 4000 m. The wet tear length corresponds to the (theoretical) length of a wet paper web in which the web would tear under its own weight. The wet tear length is ascertained as described in the examples.

The paper/tissue paper/nonwoven according to the invention preferably has a width-related breaking strength in the wet state of preferably more than 1.25 N/15 mm, greater preference being given to more than 3.5 N/15 mm and most preference being given to more than 13 N/15mm. The values refer to the measuring technique described in the examples.

The paper/tissue paper/nonwoven according to the invention has a width-related breaking strength in the dry state of preferably more than 20 N/15 mm, particularly more than 25 N/15 mm. The values refer to the measuring technique described in the examples.

The absolute strength values achieved may vary for example in accordance with the selected starting product (e.g. pulp), the basis weight of the paper/tissue paper/nonwoven, the type and quantity of the oxidizing agent and the oxidation conditions. In each case, however, the invention makes it possible to increase the absolute and relative wet strength as compared to untreated cellulosic fibrous material, particularly pulp. Relative wet strength is the quotient from the wet tensile strength and the dry tensile strength and indicates the extent to which a paper/tissue paper or paper product/tissue product retains its strength after being moistened with water. The

relative wet strength preferably amounts to more than 10%, particularly more than 15%. Even greater preference is given to values of more than 20% or more than 40%. The values refer to the measuring technique described in the examples.

Without prior mechanical treatment (beating), the WRV (water retention value) of the lignocellulosic fibrous material used to produce the paper preferably amounts to 50 - 250%, particularly 100 - 160%. The WRV was calculated as indicated in the examples.

PAPER/TISSUE PAPER/NONWOVEN PRODUCT  
ACCORDING TO THE INVENTION

The paper/tissue paper/nonwoven product according to the invention comprises at least one ply of the paper/tissue paper/nonwoven according to the invention. It is preferably a hygiene paper product, particularly a tissue product. Tissue products often contain one or more plies, preferably 1-10 plies, greater preference being given to 2 to 6, particularly 2 to 4 plies.

The tissue product is preferably

- a cleaning wipe, e.g. paper wipe, a windscreen cleaning wipe, a cleaning wipe for industrial applications, a towel or a cleaning wipe for household use, e.g. kitchen paper;
- a sanitary product, e.g. toilet paper (also moist);
- a paper handkerchief (also moist);
- a household towel, e.g. kitchen towels;
- a towel;
- a tissue for facial use, e.g. a makeup removal tissue (facial) or cosmetic tissue,
- a serviette/napkin,
- bed linen;

- a garment, e.g. disposable apparel for hospitals or kitchen staff.

Toilet paper, paper handkerchiefs and cosmetic tissues may be refined by lotioning, e.g. by application of lotions containing softness-enhancing and/or skin-care or other active cosmetic ingredients

The paper/tissue paper/nonwoven product according to the invention, particularly tissue product, may exist as a sheet, single sheet or as a roll, optionally divided into sheets. It may be folded or unfolded, embossed or unembossed, printed or unprinted, perforated or unperforated and/or it may have undergone finishing e.g. by application of lotions.

In the case of single-ply products, the mechanical properties of the paper/tissue product/nonwoven product correspond to the above-indicated values. The strength values increase as the number of plies rises.

The paper/tissue product/nonwoven product according to the invention preferably has the aforementioned basis weights in the case of just one ply. If there are several plies, the basis weight correspondingly rises with the number of plies.

#### METHOD OF PRODUCING THE FIBROUS MATERIAL ACCORDING TO THE INVENTION, THE PAPER/TISSUE PAPER/NONWOVEN AND THE PAPER/TISSUE PAPER/NONWOVEN PRODUCT

The production of the fibrous material according to the invention entails the oxidation of the OH functions at the glucose C(6) of the cellulose in cellulose-containing fibers into aldehyde groups (to increase wet strength) and/or carboxy groups (to increase dry strength).

The pulp density of the fibers used for oxidation usually amounts to 0.05 to 30%, particularly 0.05 to 5%, expressed as

the dry weight of the fibers (oven-dried) per weight of the medium. The oxidizing medium is preferably aqueous; other oxidizing media, e.g. combinations of water and a water-miscible solvent, e.g. alcohol, can also, however, be used so long as the water-miscible solvent is not attacked by the oxidizing agent.

The amount of oxidizing agent is preferably 0.005 to 70 wt.%, particularly 0.05 to 50 wt.%, greater preference being given to 0.05 to 30 wt.%, particularly 0.05 to 15 wt.%, relative to the dry weight (oven-dried) of the fibrous material.

Depending on the oxidizing agent in use, oxidation is preferably performed at a temperature of 1°C to 120°C, particularly 1 to 50°C. The reaction time preferably amounts to 5 min to 15 hours, particularly 30 min to 7 hours.

A combination of reaction conditions (concentration, pH, temperature, reaction duration etc.) which does not result in the destruction of the fibrous structure is preferably chosen. Individual examples of the combination of such conditions will be explained below with the corresponding oxidizing agents.

Oxidation of the starting material may be effected with any oxidizing agent that oxidizes the OH functions at the C(6) of the glucose unit of the cellulose (for the sake of simplicity, just "C(6)" will be referred to hereinafter) into aldehydes and/or carboxyl groups. Suitable oxidizing agents are for example ozone, periodate, dinitrogen tetroxide ( $N_2O_4$ ), dimethyl sulfoxide/acetic anhydride, gaseous oxygen, hypochlorite, hypobromite, chromic acid and chromates, hypochlorous acid, hypobromous acid, hypoiodous acid, peracids, peroxides (e.g. hydrogen peroxide), persulfates, perborates, perphosphates, periodates, oxidizing metal compounds, nitroxy compounds, particularly the so-called TEMPO oxidizing systems, and suitable combinations thereof. Halogen-free oxidizing agents are preferred.

Upon oxidation with dinitrogen tetroxide, C<sub>6</sub> carboxyl-functionalized cellulose is formed as the main product and C(2,3) dialdehyde, C(2,3) dicarboxyl and C(2,3) diketone groups are formed as a by-product, whereby further forms of oxidation are not excluded.

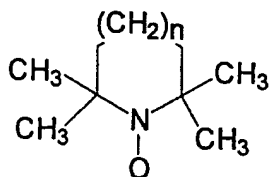
Dinitrogen tetroxide has the ability to react not only with the hydroxy groups located on the surface of the groundwood fiber and/or particularly the pulp fiber, but also penetrates into the interior of the fiber structure without destroying the fibrous structure. Oxidation on the fiber surface is preferred, however, which can be achieved in that the lumen of the pulp fibers is reduced by compression before and/or during oxidation.

Sodium hypochlorite as a sole oxidizing agent leads to a very low carboxyl content under mildly acidic conditions and results in higher carboxyl contents under alkaline conditions, though the oxycelluloses obtained under mildly acidic conditions tend toward a yellow coloration and to degradation.

A sterically hindered organic nitroxy compound is preferably used. One, particularly two bulky groups in the  $\alpha$  position to the NO is/are suitable for sterical hindrance of the NO group, e.g. optionally substituted phenyl or aliphatic substituents that are linked to the nitrogen atom of the NO by a quaternary C atom, e.g. tert-butyl. Two substituents can also be combined into an alkenyl unit optionally interrupted by a hetero-atom (e.g. O,N) (to form an alicyclic or heterocyclic ring).

Oxidation with nitroxy compounds usually leads, via the aldehyde function, to the carboxy function, the choice of oxidizing system and oxidation conditions making it possible to control the reaction such as to isolate the aldehyde stage. The proportion of carboxy groups usually rises as the reaction duration increases.

Preferred oxidation systems can be represented by the following formula I



(I)

where  $n = 0$  or  $1$  and where the methylene groups of the ring may carry one or more substituents selected from alkyl, alkoxy, aryl, aryloxy, amino, amido (e.g. acetamido, 2-bromacetamido and 2-iodacetamido), oxo, cyano, hydroxy, carboxyl, phosphonooxy, maleimido, isothiocyanato, alkyloxy, fluorophosphinyloxy (particularly ethoxyfluorophosphinyloxy), substituted or unsubstituted benzoyloxy, e.g. 4-nitrobenzoyloxy. If  $n = 1$  (i.e. the ring represents a piperidine), these groups preferably substitute the 4-position of the piperidine. The di-tert.-alkyl nitroxy unit can also be present as part of a polymer structure such as  $\{(\text{CH}_3)_2\text{-C-(CH}_2)_2\text{-C-(CH}_3)_2\text{-C-NO-}\}_m$ . Hydroxy, amino and amido are preferred among these substituents on account of the stability of the nitroxy compound under acidic conditions.

An example of  $n=0$  is PROXYL (2,2,5,5-tetramethylpyrrolidine-N-oxyl).

Among the formula I compounds, the case of  $n=1$  is preferred. This leads to the optionally substituted TEMPO compounds (2,2,6,6-tetramethyl-4-piperidine-N-oxide) which can selectively oxidize the primary hydroxy group at C(6) of the glucose unit of the cellulose into aldehyde and/or carboxyl groups.



The nitroxy compound can be used stoichiometrically or in combination with a primary oxidizing agent capable of returning the nitroxy compound to the oxidized state after its consumption (reduction) (a list of suitable reaction conditions and compounds is found in A.E.J. De Nooy, Synthesis 1996, 1153-1174). The pH range of the reaction generally varies between 1 and 14, preferably 2 and 7, particularly 3 and 6. The reaction temperature is preferably between 5°C and 80°C. The nitroxy compound may be added to a suspension of the fibrous material as a solid (also as a pasty substance) or as a solution (usually as an aqueous solution).

In the second case (nitroxy compound + primary oxidizing agent), preferably first the nitroxy compound and then the primary oxidizing agent is added. The oxidizing agent can be added all at once or distributed over the duration of the reaction (e.g. by evenly adding it in drops). The primary oxidizing agent (e.g. peracetic acid, ozone, hypohalite, metal compounds that contain oxygen) is preferably used in an amount of 0.1 to 20 wt.%, particularly 0.5 to 7.5 wt.%, in relation to the dry weight (oven-dried) of the fibrous material. The catalytic quantity of the nitroxy compound is preferably 0.05 to 15 wt.% relative to the dry weight (oven-dried) of the fibrous material.

In the case of stoichiometric reaction with the nitroxy compound, this compound is used in an amount of 0.005 to 70 wt.%, particularly 0.05 to 50 wt.%, greater preference being given to 0.05 to 30 wt.%, particularly 0.05 to 15 wt.%, relative to the dry weight (oven-dried) of the fibrous material.

One version of performing the oxidation with the formula I nitroxy compound is described in WO 95/07393 which teaches the oxidation with a catalytic amount of the nitroxy compound and a hypohalite (e.g. NaOCl) as a primary oxidizing agent in an aqueous reaction medium at a pH between 9 and 13. Under these

conditions, the primary hydroxy group of the cellulose is oxidized via the corresponding aldehyde group into the carboxyl group.

A preferred version lies in the oxidation with a peracid, a precursor or a salt thereof as a primary oxidizing agent in the presence of a catalytic amount of the nitroxy compound (particularly optionally substituted TEMPO) and a catalytic amount of a halide (e.g. NaBr), preferably in the pH range of 2 to 11, particularly 2.5 to 3.5. The halide is preferably used in a quantity of 0.1 to 40, particularly 0.5 to 10 mol% relative to the hydroxy groups. The nitroxy compound is preferably used in a quantity of 0.1 to 2.5 wt.%, relative to the dry weight (oven-dried) of the fibrous material. The peracid is preferably a peralkanic acid, particularly peracetic acid. Depending on the reaction duration, this embodiment of oxidation leads to aldehydes and/or carboxyl groups at C(6) of the glucose unit of the cellulose. It is, however, also possible to perform oxidation just using the nitroxy compound (particularly the formula (I) compound) as a mediator and peracid as an oxidizing agent without halide, particularly bromide

Another preferred version lies in the combination of a catalytic amount of the nitroxy compound (particularly optionally substituted TEMPO) and a suitable oxidic compound of a metal of the transition metals of periods Va to VIIa in the oxidation state of at least +3, e.g. oxides and oxygen-containing ions of manganese, chromium, iron, nickel, ruthenium and vanadium, e.g. vanadium pentoxide, iron oxide, chromium (VI) oxide, chromates and particularly manganese (IV) oxide and salts of permanganic acid. The reaction is preferably conducted at a pH between 2 and 8. The nitroxy compound is preferably used in an amount of 0.1 to 2.5 wt.%, relative to the dry weight (oven-dried) of the fibrous material. The reaction temperature is preferably less than 80°C, particularly 30 to 60°C. Depending on the duration of

the reaction, this embodiment of the oxidation leads to aldehydes and/or carboxyl groups at C(6). In a preferred version of this embodiment, the primary oxidation step, i.e. oxidation of the cellulose by the nitroxy compound, can be separated from the secondary oxidation step, i.e. oxidation of the reduced nitroxy compounds by the oxygen-containing metal compound. The oxidation of the cellulose-containing fibrous material (e.g. pulp) can therefore be performed in a first reactor, the discharge from the first reactor can be separated from the oxidized fibers and introduced into a second reactor where it is treated with the insoluble or immobilized metal compound (e.g. a manganese (IV) oxide bed). The metal compounds can then be filtered off and the filtrate guided to the first reactor in a circulating manner. Such methods can also be conducted in a semicontinuous or continuous mode.

Another preferred version lies in the oxidation of the cellulose with a catalytic amount of the formula I nitroxy compound that is hydroxy-, amino- or amido-substituted (e.g. 4-hydroxy TEMPO) at a pH between 1 and 7, particularly 2 to 6. In this version, a hypohalite (e.g. NaOCl) or ozone is particularly suitable as a primary oxidizing agent. The nitroxy compound is preferably used here in an amount of 0.05 to 15 wt.% and the primary oxidizing agent in an amount of 0.1 to 20 wt.%, each relative to the dry weight (oven-dried) of the fibrous material. The reaction temperature is preferably 5 to 50°C. Depending on the reaction duration, this embodiment of oxidation results in aldehydes and/or carboxyl groups at C(6) of the glucose unit of the cellulose. Halogen-free acids, such as sulfuric acid or toluene sulfonic acid, are particularly suitable for setting the pH.

Finally, the nitroxy compound can also be used with enzymes and/or metal complexes. In this embodiment the catalytic amount of the nitroxyl compound is preferably 0,1-2,5 mol% with respect to the C(6)-alcohol to be oxidized.

The catalysts to be used according to this embodiment are oxidoreductases or other enzymes that are capable of oxidation in the presence of a suitable redox system. Oxido-reductases, i.e. enzymes capable of oxidation without the presence of further redox systems, to be used include peroxidases and oxidases, in particular polyphenol oxidases and laccase. Certain hydrolases, such as phytase, can be used when a further redox system is present such as a metal complex, e.g. vanadate. Metal complexes as such, without an enzyme protein, can also be used; examples include copper and iron complexes with porphyrins, phenanthrolins, polyamines such as EDTA, EGTA and the like. The metal-assisted enzymes and metal complexes require hydrogen peroxide, alkyl and ar(alk)yl hydroperoxides (such as tert-butyl hydroperoxide) or chlorite as an ultimate electron acceptor. Peroxidases (EC 1.11.1.1 - 1.11.1.11) that can be used according to the invention include the peroxidases which are cofactor-independent, in particular the classical peroxidases (EC 1.11.1.7). Peroxidases can be derived from any source, including plants, bacteria, filamentous and other fungi and yeasts. Examples are horseradish peroxidase, soy-hull peroxidase, myelo peroxidase, lactoperoxidase, *Arthromyces* and *Coprinus* peroxidases. Several peroxidases are commercially available. The peroxidases require hydrogen peroxide as an electron acceptor. Polyphenol oxidases (EC 1.10.3.1.) include tyrosinases and catechol oxidases such as lignine peroxidase. Suitable polyphenol oxidases may be obtained from fungi, plants or animals. The polyphenol oxidases require oxygen as an electron acceptor. Laccases (EC 1.10.3.2) are sometimes grouped under the polyphenol oxidases, but they can also be classified as a distinct group, sometimes referred to as p-diphenol oxidases. The laccases can be derived from plant sources or from microbial, especially fungal, sources. The laccases also require oxygen as an electron acceptor. The process for producing the aldehydes according to this embodiment can be performed under relatively mild conditions, e.g. at a pH between 2 and 10, and at a temperature between 15 and 60°C (both depending on the

particular enzyme or metal complex). The reaction medium can be an aqueous medium, or a homogenous mixed medium, e.g. a mixture of a water and a water-immiscible organic solvent such as a hydrophobic ether, a hydrocarbon or a halogenated hydrocarbon. In the latter case, the enzyme and/or the nitroxyl and the oxidising agent may be present in the aqueous phase and the alcohol substrate and the aldehyde or ketone product may be present in the organic phase. If necessary, a phase transfer catalyst may be used. The reaction medium can also be solid/liquid mixture, in particular when the enzyme of the nitroxyl are immobilised on solid carrier. A heterogeneous reaction medium may be advantageous when the substrate or the product is relatively sensitive or when separation of the product from the other reagents may present difficulties.

Further in particular amido-substituted nitroxy compounds (e.g. 4-acetamido TEMPO) of the aforementioned formula I are suitable for stoichiometric oxidation at a pH between 1 and 7, particularly 2 to 6, particularly 2 to 3. In this reaction, halogen-free acids such as sulfuric acid or toluene sulfonic acid are particularly suitable for adjusting the pH. Under these conditions, the nitroxy compound present as a radical disproportionates into an oxammonium ion that acts as an oxidizing species and a hydroxylamine. After the reaction, the consumed (reduced) form of the nitroxy compound can be regenerated with ozone or another oxidizing agent, preferably in a separate process step. An important advantage of the oxidation version discussed here is the ability to use the choice of a suitable pulp (TCF, see following sections) to conduct the entire paper/tissue-paper/nonwoven production method without any halogen-containing chemicals.

After treatment with the oxidizing agent/system, the thus treated fibrous material can be used either directly or further diluted (diluted to the pulp densities of 0.1 to 1% usual during paper production in the headbox). It is

advantageous, however, for the oxidizing agent and any optionally used oxidizing auxiliary substances (e.g. catalysts such as the nitroxy compound) to be removed from the fibers by washing in a separate process step. This may occur by using scrubbers common in pulp production in a displacement or dilution wash. After washing, the fibers can be thickened to a higher pulp density or pressed out by means of usual apparatus (e.g. filters, wash filters, filter presses or other drainage devices). It may optionally be of advantage to destroy the oxidizing agent or oxidizing auxiliary substances by chemical means before washing the fibers. For example, excess hypochlorite can be destroyed by reaction with hydrogen peroxide, thus preventing the hypochlorite from reaching the washing stage.

To explain in more detail the preferred raw materials used in the fiber production process and the preferred times at which oxidation is performed during the production of paper/tissue paper/nonwovens, a typical production process for paper/tissue paper/nonwoven products will first be discussed more closely. This method is usually classified into different process steps, for example for pulps as a starting material (the same applies to fibrous materials):

1. production of the pulp modified by oxidation based on raw pulps exhibiting properties adapted to paper/tissue paper/nonwoven production, including the pulp refinement common in the paper production process;
2. processing (including formation, i.e. sheet laying and drying) of the modified pulps into a paper/tissue paper/nonwoven;
3. processing this paper/tissue paper/nonwoven into a paper product/tissue product/nonwoven product.

Upon adjustment of the properties of the pulps recovered from wood by means of normal chemical pulping techniques (e.g. kraft process; sulfite process) in step 1, one or more of the following steps are frequently applied:

(1a) a separating step by fractionating, sorting, washing, floating and/or cleaning (in a fractionating device, a sorting device, a washing device, a floatation cell or a hydrocyclone or another cleaning device)

(1b) dispersing and thickening steps in a dispersing device or e.g. a screen head extruder or screw press

(1c) dissolving the fibers (pulping) by deflaking/fiberizing, e.g. in a pulper or fiberizer, a dispersing apparatus or a sorting device

(1d) fiber modification in a refiner or other type of beating unit or a pump

(1e) storage steps, mixing and dilution steps.

If e.g. linters or cotton is used as a raw material for the production of paper/tissue paper/nonwovens, no further pulping steps are usually needed, however. Due to the morphological structure, the cellulose already exists in an open state.

The starting pulps in use for oxidation may relate to primary fibrous materials (raw pulps) or to secondary fibrous materials, whereby a secondary fibrous material is defined as a fibrous raw material recovered from a recycling process. The primary fibrous materials may relate both to a chemically digested pulp and to mechanical pulp such as thermorefiner mechanical pulp (TMP), chemothermorefiner mechanical pulp (CTMP) or high temperature chemithermomechanical pulp (HTCTMP). Synthetic cellulose-containing fibers can also be used. Preference is nevertheless given to the use of pulp from plant material, particularly wood-forming plants. Fibers of

softwood (usually originating from conifers), hardwood (usually originating from deciduous trees) or from cotton linters can be used for example. Fibers from esparto (alfa) grass, bagasse (cereal straw, rice straw, bamboo, hemp), kemp fibers, flax and other woody and cellulosic fiber sources can also be used as raw materials. The corresponding fiber source is chosen in accordance with the desired properties of the end product in a manner known in the art. For example, the fibers present in softwood which are shorter than those of hardwood lend the final product a higher stability on account of the higher diameter/length ratio. If the softness of the product is to be promoted, which is important e.g. for tissue paper, eucalyptus wood is particularly suitable as a fiber source.

With regard to the softness of the products, the use of chemical raw pulps is also preferred, whereby it is possible to use completely bleached, partially bleached and unbleached fibers. The chemical raw pulps suitable according to the invention include, inter alia, sulfite pulps, kraft pulps (sulfate process), soda pulps (cooking with sodium hydroxide), pulps from high-pressure cooking with organic solvents (e.g. Organosolv, Organocell, Acetosolv, Alcell) and pulps from modified processes (e.g. ASAM, Stora or Sivola process). Among the kraft pulps, it is possible to use those which were obtained in continuous cooking systems (MCC (modified continuous cooking), EMCC (extended modified continuous cooking) and ITC (isothermal cooking)). The products of discontinuous kraft processes (e.g. RDH (rapid displacement heating), Superbatch and Enerbatch) are also suitable as a starting product. The sulfite processes include the acidic sulfite/bisulfite processes, bisulfite process, "neutral sulfite semi-chemical pulping" (NSSC) process and alkaline sulfite processes such as processes in which in addition to aqueous alkali, sulfite and/or anthraquinone in combination with organic solvents such as methanol were used for cooking, e.g. the so-called ASAM process (alkali sulfite anthraquinone methanol). The major difference between the acidic and neutral



or alkaline sulfite processes is the higher degree of delignification in acidic cooking processes (lower kappa numbers). The NSSC process provides semi-chemical pulps which are advantageously defibered in downstream mechanical fibrillation before they are used according to the invention for the purpose of oxidation. The sulfite and kraft pulps considerably differ in terms of their fibrous material properties. The individual fiber strengths of sulfite pulps are usually much lower than those of kraft pulps. The mean pore width of the swollen fibers is also greater in sulfite pulps and the density of the cell wall is lower compared to sulfate pulps, which simultaneously means that the cell-wall volume is greater in sulfite pulps. For this reason, there are also obvious differences regarding water absorption and swelling behavior of the cellulosic fibrous materials, which must also be taken into consideration when selecting the raw material for oxidation.

Before a raw pulp is oxidized in the process according to the invention, it may also be advantageous to allow further delignification to occur in a separate process step.

In this way, for example, pulps which

- were cooked in alkaline pulp production techniques such as the kraft process or ASAM process
- were cooked in acidic pulp production techniques such as the acidic magnesium bisulfite process, and/or
- originate from processes in which organic solvents such as methanol (e.g. Organosolv, Organocell, Acetosolv, Alcell) were used

should undergo a bleaching process to achieve a more extensive removal of lignin after the cooking process and to obtain a completely cooked pulp.

In this bleaching process, elementary chlorine or chlorine-containing bleaching chemicals such as chlorine dioxide ( $\text{ClO}_2$ ) or hypochlorite ( $\text{OCl}^-$ ) can be used, although this is not preferred for ecological and strategic marketing

reasons. Bleaching with oxygen, hydrogen peroxide or the joint use of oxygen and hydrogen peroxide, not to mention ozone or an oxygen/ozone and/or air/ozone/gas mixture is therefore particularly suitable. Bleaching with peracetic acid is also suitable as a bleaching agent that contains oxygen, it being irrelevant whether it is a question of equilibrium peracetic acid or distilled peracetic acid. Caro's acid can also be used as a peroxide chemical under acidic pH conditions for the purpose of bleaching. The avoidance of chlorine-containing bleaching chemicals produces ECF (elemental chlorine free) or TCF (total chlorine free) pulps which are preferred according to the invention. In addition to the bleaching agent, reducing bleaching agents such as dithionite ( $S_2O_4^{2-}$ ) or foramidine sulfonic acid (FAS) can be used to brighten the fibrous material. It should be mentioned here that the use of these bleaching chemicals, particularly when using ozone or ozonized oxygen or an ozone/air mixture, may, to a slight extent, also result, as a side reaction, in the formation of carboxyl and carbonyl groups in the cellulose chain. This nevertheless only leads to a smaller increase in static strength properties, but a significant improvement regarding wet strength is not usually observed. A useful increase in the wet strength of paper products therefore cannot be achieved by just oxidizing the fibrous material with the aforementioned oxidizing agents.

It is also preferred that before oxidation, the chemical pulp should undergo additional surface treatment (beating) which has a favorable effect on the strength properties of the obtained paper/tissue paper/nonwoven product. This may be preferably brought about within the pulp refinement system of a paper/tissue paper machine. In another preferred embodiment, such surface treatment (beating) occurs as part of pulp production, i.e. while it is still at the pulp plant. A refiner is particularly suitable for this purpose. Fibrillation of the surface occurs during mechanical treatment of the pulp/water suspension. This treatment affects the static and dynamic strength properties. Fibrillability of the

fiber crucially depends on the fiber's swelling capability. In this way, it is known that due to a low polyuronic acid content, kraft pulps produced according to the sulfate process are less readily beatable. Effects of beating in accordance with e.g. the specific edge load, total energy expenditure etc. are discussed in detail by the following authors: Lothar Göttsching, *Stofftechnologie - Mechanische Faserbehandlung; Wochenblatt für Papierfabrikation* 23/24, (1998), 1194; M.L. Wild, *Festigkeitsentwicklung von Holz- und Deinkstoff aus Zeitungsdruckpapier mit niedriger spezifischer Kantenbelastung; Wochenblatt für Papierfabrikation* 23/24, (1998), 1218. The bleaching of fibrous materials containing lignocellulose also considerably affects their grindability and the beating result.

(Jorma Lumiainen, *Refinermahlung von ECF-, TCF- und chlorgebleichten Zellstoffen unter äquivalenten Bedingungen*, *apv (Allgemeiner Papier Rundschau)*, 33 (1998), 768).

Fibrillation of the fibers during beating occurs either by the fibers themselves or by the refiner knives. During beating, the fibers are subjected to a variety of physical loads. Axial and tangential shearing and compressive forces acting upon the fiber play a particular role as regards fiber reforming. This leads to a change in fiber morphology. In this way, the outer primary wall is the first to be separated. The associated change in fiber morphology can be described as follows:

- a) tearing open and removing the fibrous material's outer wall layer designated as the primary wall;
- b) exposing the fibrils and fibrillation out of the wall layers designated as S1 and S2;
- c) partially shortening the total fiber unit or producing accepts by shearing off fibrils.

The beating effect is also determined by the hemicelluloses which influence beating as a result of the amorphous structure and their easy swelling capability. A phenomenon known in the

formation of nonwovens is the so-called Campbell effect that describes how the fibrils come closer during nonwoven formation. As soon as so much water is removed from the nonwoven that the fibrils come closer and capillarity occurs, they are pressed together as a result of the capillary pressure and form hydrogen bridges (secondary valence forces) in the course of drying. The hemicelluloses with water as a polar liquid may also lead to the formation of a gel that causes the fibers to agglutinate.

The influences of the cutting angle of the ribs and grooves attached to the beating unit in relation to the change in characteristic of the fibrous material are described in *PTS Research Report: G. Bär, Faserstoffoptimierung durch modifizierten Mahlprozess PTS-FB 19/98, 1st edition, (1998)*.

Depending on the refiner's operating mode, the fibers are shortened (cut) or are fibrillated, which includes the separation of the outer layers of the fiber wall, this latter process substantially increasing the surface and bonding capacity of the fibers. The refiner operating mode that accompanies fibrillation is therefore preferred (to simplify matters, this process step will also be designated as beating in the following). Beating is particularly used in the case of chemical pulps.

It is preferred that neither the raw pulp, as is obtained e.g. from any kind of pulping process, nor a completely wood-free cellulosic fibrous material should undergo drying before it is supplied to the stage in which paper/tissue paper/nonwoven is formed. This makes it possible to perform oxidation of the fibers in a completely swollen state. So long as the oxidation reaction has not already occurred to a sufficient extent during bleaching, or the introduction of other groups is desirable, it is therefore possible to continue oxidation in the swollen state. In accordance with the prior art, the raw pulp or final pulp is usually first brought into the air-dried state and not until directly before processing into a

paper/tissue paper/nonwoven product is it brought into a water-saturated state. In this way, storable pulps are obtained which do not have to be processed immediately after the production process. Due to the effect known as drying hysteresis, however, the swelling state that can be achieved before drying is no longer achieved upon re-moistening. As a result, the accessibility of the fibers for the oxidizing agent is decreased. If the pulp is consequently not dried in the above-described special embodiment of the invention, the accessibility of the fibers for the oxidizing agent is increased and an additional rise in wet strength can be achieved.

Depending on the type of paper, the second process section (paper/tissue paper/nonwoven formation) may include the typical process steps of sheet making: pressing, drying, sizing (in the case of paper production) and smoothing (calendering).

If tissue paper is to be made, process section 2 essentially comprises

- 2a forming that includes the headbox and the screen portion,
- 2b the drying portion (TAD (through air drying) or conventional drying on the yankee cylinder) that also usually includes the crepe process essential for tissues,
- 2c the monitoring and winding area.

Formation of the paper can be achieved by placing the fibers, in an oriented or random manner, on one or between two endlessly revolving screens of the paper making machine while simultaneously removing the main quantity of water of dilution until dry-solids contents of usually between 12 and 35%.

Drying the formed primary fibrous web occurs in one or more steps by mechanical and thermal means until a final dry-solids content of usually about 93 to 97%. In the case of tissue making, this stage is followed by the crepe process which crucially influences the properties of the finished tissue product in conventional processes. The dry crepe process that is predominantly in use today involves creping on a usually 4.5 to 6 m diameter drying cylinder, the so-called yankee cylinder, by means of a crepe doctor in the case of the aforementioned final dry-solids content of the raw tissue paper (wet creping can be used if lower demands are made of the tissue quality). In the next step, the creped, finally dry raw tissue paper (raw tissue) is then usually wound on to a supporting core to form a so-called reel drum or is wound in a longitudinally cut manner on cores to form master rolls and is available in this form for further processing into the paper product or tissue paper product according to the invention.

Instead of the conventional tissue making process described above, the invention gives preference to the use of a modified technique in which an improvement in specific volume is achieved by a special kind of drying within process section 2b and in this way an improvement in the bulk softness of the thus made tissue paper is achieved. This process, which exists in a variety of subtypes, is termed the TAD (through air drying) technique. It is characterized by the fact that the "primary" fibrous web that leaves the sheet making stage is pre-dried (like a nonwoven) to a dry-solids content of about 80% before final contact drying on the yankee cylinder by blowing hot air through the nonwoven fabric. The nonwoven fabric is supported by an air-permeable screen or belt and during its transport is guided over the surface of an air-permeable rotating cylinder drum. Structuring the supporting screen or belt makes it possible to produce a random pattern of compressed zones broken up by deformation in the moist state, resulting in increased mean specific volumes and consequently leading to an increase in crumple softness

without decisively decreasing the strength of the nonwoven fabric. Another possible influence on the softness and strength of the raw tissue lies in the production of a layering in which the primary nonwoven fabric to be formed is built up by a specially constructed headbox in the form of physically different layers of fibrous material, these layers being jointly supplied as a pulp strand to the sheet making stage. The surface softness can be significantly increased by suitably selecting the raw materials in the headbox outlet nozzle channels that determine the layering, for example by using eucalyptus fibers and/or wattle, at the nonwoven side facing toward the yankee cylinder surface, which benefits the products manufactured from raw tissue production.

When processing the raw nonwoven or raw paper into the final product (third process section), the following procedural steps are normally used individually or in combination: cutting to size (longitudinally and/or cross cutting), cutting to size, producing a plurality of plies, producing mechanical ply adhesion, volumetric and structural embossing, application of adhesive, folding, imprinting, perforating, application of lotions, smoothing (calendering), stacking, rolling up.

To produce multiply tissue papers, such as handkerchiefs, toilet paper, towels or kitchen towels, an intermediate step preferably occurs with so-called doubling in which the raw tissue is usually unwound in a reel drum number corresponding to the finished product's desired number of plies and is wound on a common multiply master roll. This processing step frequently includes smoothing or calendering in two-roll or multi-roll calenders. After completion of drying and creping, smoothing (calendering) may also, however, be performed in the tissue machine directly before reeling up.

The processing step from the raw tissue that has already been optionally wound up in several plies to the finished tissue product occurs in special purpose-built processing machines

which include operations such as repeated smoothing of the tissue, edge embossing, to an extent combined with planar and/or local application of adhesive to produce ply adhesion of the individual plies (raw tissue) to be combined together, as well as longitudinal cut, folding, cross cut, placement and bringing together a plurality of individual tissues and their packaging as well as bringing them together to form larger surrounding packaging or bundles. Instead of edge embossing, the production of ply adhesion can also be achieved by edging, as is common e.g. in the case of cosmetic tissues. The individual paper ply webs can also be pre-embossed and then combined in a roll gap according to the foot-to-foot or nested methods.

Timing of oxidation: with regard to the consumption of oxidizing agent, it is preferred that oxidation should be performed on as pure fibrous material as possible (having as high a cellulose content as possible). Oxidation of the fibers therefore preferably occurs during process section 1, tending to be performed here at the end of process section 1, e.g. directly before laying the sheets.

If there is a desire to confer antibacterial properties upon the cellulose-containing fibrous material, this material can be treated with an antibacterial agent at a suitable point in time, as is described in EP-A-905 289. A silver-based antibacterial agent is preferably used, e.g. silver zeolite, silver zirconium phosphate, silver calcium phosphate or silver-soluble glass. Silver zirconium phosphate can also be simultaneously used to crosslink the oxidized fibrous material. The treated fibrous material preferably contains the antimicrobial agent in an amount of 0.1 to 25.0 wt.%, particularly 0.1 to 0.5 wt.%, relative to the treated fibrous material (oven-dried). The treated fibrous material is suitable for example for the manufacture of medical products such as bandages, gauze, garments for surgical purposes or bed linen for hospital use.



The application of the modification - in accordance with the invention - of the fibrous materials by oxidation is possible in numerous versions, a few of which will be illustrated below by way of example, without any claim to completeness.

- In principle, the modification of fibers in accordance with the invention, particularly the modification of the outer fiber surface by oxidation, can be applied to any raw fibrous material that contains lignocellulose, particularly any natural vegetable raw fibrous materials. This is true inasmuch as these raw fibrous materials are suitable for example as raw material for the fiberboard industry, e.g. for the production of medium-density fiberboards, as a raw material for the paper industry for the production of paper, cardboard and board exhibiting a wide variety of basis weights according to the wet-laying techniques normally used for this purpose, particularly in the production of raw tissue or can be used for the production of nonwovens according to the wet-laying or various dry-laying techniques or in the production of fluff products, e.g. in hygiene products.
- The invention is in principle suitable for application in a wide variety of industrial production sectors such as pulp production, paper and especially tissue paper production, paper and especially tissue processing, not to mention the production of nonwovens or quite different fields such as fiberboard production, particularly the production of medium-density fiberboards, without wishing to be restricted to these areas of application.
- Besides starting and intermediate products, particularly planar intermediate products, the invention covers any finished products whose production entails the use of the aforementioned fibrous materials containing lignocellulose and modified by oxidation either proportionally or on their

own, optionally in combination with additives and/or auxiliary substances.

The finished products for end-user consumption particularly include any categories of hygiene product - particularly any kinds of tissue product for hygiene requirements in the "consumer" sector and for "institutional" needs.

- Within pulp production, the modification of fibrous material by oxidation of the primary hydroxyl group of the C6 atom on the glucose rings of the cellulose chain molecules, preferably the fiber wall, particularly at those of the easily accessible outer fiber wall, may become important in its own right by integrating this modification into pulp production as a separate process step in the form of an optionally additional refining stage.

As defined by the invention, the term pulp production includes any technology or processes that can be used to recover cellulose-containing fibrous materials from raw vegetable materials which are then suitable as a raw fibrous material for the production of planar materials, optionally composite planar materials, such as paper especially tissue paper, cardboard, board, fiberboards, nonwovens and the like.

It is irrelevant whether the decomposition of the vegetable fiber composite (cell unit, e.g. the ligneous substance of suitable types of wood) into useful single fibers is performed by chemical pulping, which depending on the degree of pulping (yield) leads to the chemical pulps and semi-chemical pulps, or whether pulp production is brought about by mechanical means by expending mechanical energy and/or heat energy optionally by also using chemicals that assist the pulping process, such as chippings of suitable kinds of wood, which leads to the group of mechanical pulps including for example groundwood pulp, TMP, CMP, CTMT, HTCTMP and other mechanical pulps.

It is important that the chemical pulps derived from plant fibers (cells) predominantly comprise cellulose and hemicelluloses having a residual lignin content dependent on the pulping process, degree of pulping and bleaching, the other accompanying substances such as waxes and minerals being of secondary importance.

In contrast, the mechanical pulps are characterized by their very high lignin content, because again in accordance with the pulping process, e.g. in the case of groundwood pulp, MP or TMP, the original lignin content characteristic of the plant is de facto retained or decreases only to a slight extent if thermal and/or chemical energy is additionally applied.

- A first embodiment of the invention provides the inclusion of a refining stage suitable for implementing the modification of the fibrous material, e.g. by oxidation, as an integral component of pulp production.

This refining stage is equipped with all the apparatus needed to perform the modification of the fibrous material, as stated above and described below in another part of the specification text, and in the case of chemical pulp production, is embedded into the overall process of pulp production at a suitable point, for example during bleaching in combination with washing.

As a result, a modified fibrous material or a modified pulp is obtained which can be used for example as a starting product for paper production.

Such a fibrous material according to the invention (e.g. chemical pulp) may, in a further embodiment, exist as a special type of commercial pulp dried e.g. in sheet form, stacked into bales or pressed into bales having been air-dried, optionally also flash-dried.

A third embodiment is obtained by offering the modified fibrous material (e.g. a chemical pulp) in undried form as a liquid pulp so that it is in readiness for example in a

so-called integrated pulp and paper or tissue plant directly as a starting product for paper and especially tissue paper production, optionally with subsequent processing.

Availability as a liquid pulp is particularly advantageous because the properties' higher potential gained by the modification has an effect here without any losses, particularly the potential to improve physical properties, e.g. that of the initial wet strength of a planar material made of this modified fibrous material, such as the initial wet strength of a paper made thereof, particularly a tissue paper, whereas drying the fibrous material, e.g. as a result of further oxidation of the carbonyl groups into carboxyl groups, may entail losses which prevent the potential of properties from being completely exhausted.

- It is provided in a further, particularly preferred embodiment of the invention to integrate a refining stage into the pulp refinement section of a paper machine - especially a tissue paper machine - for the modification of the fibrous materials by oxidation of the hydroxyl group of the C6 atom of the glucose units of the cellulose into carbonyl groups, in order to make fibrous raw materials suitable for paper production and particularly tissue paper production available by modification of cellulose-containing fibrous materials, particularly pulps of fibrous wood, irrespective of the pulping process, whether produced in acidic or neutral or alkaline conditions, whether produced in single-stage or multi-stage processes or whether produced with or without bleaching; the use of such fibrous raw materials in sheet making leads to paper or raw tissue which is characterized by improved strengths, particularly improved wet strength, by dimensional stability of the product, by high absorbency for liquids such as water with good textile-like flexibility of the final products made therefrom, as compared to those kinds of paper or raw tissue paper which are made of otherwise comparable, albeit

unmodified fibrous raw materials in comparable production conditions.

- In an embodiment of the invention, the total fibrous raw material supplied to a machine can be modified by oxidation within the refining stage integrated into a pulp refinement section of a paper machine, particularly a tissue paper machine.
- According to a further embodiment, however, just a partial amount of the fibrous raw material needed by a paper or tissue paper machine can optionally be modified by oxidation of the kind according to the invention and used in combination with unmodified fibrous raw material.
- Another preferred way of obtaining a starting or intermediate product according to the invention, such as an endless web of paper or raw tissue, is to keep separate the fibrous material modified by oxidation in accordance with the invention or optionally to keep the modified fibrous materials separate within the pulp refinement stage as fibrous raw materials with different properties and to guide them each in a separate channel of a multi-layer headbox and to supply the unmodified fibrous raw materials to sheet making through optionally additional parallel channels of the multi-layer headbox together with the modified fibrous raw materials in the form of a layered jet.

Interchanging the supply of raw material to the individual channels of a multi-layer headbox thus makes it possible to use the fibrous material according to the invention to influence systematically the physical properties, such as strength, especially wet strength and/or dimensional stability of the resultant product, to minimize its costs for example in that more inexpensive fibrous raw materials form the core layers of the multi-layer composite, but the

outer layers are formed by higher-quality fibrous raw materials.

Another example is the improvement in the "runnability" of a tissue machine, such as a conventionally operating tissue machine, by ensuring that a suitable fibrous raw material, such as eucalyptus pulp, forms that outer layer of the multi-layer fiber composite which comes into contact with the yankee cylinder surface.

- Other versions according to the invention are brought about in that either different fibrous raw materials are modified or one and the same fibrous raw material is varyingly modified in separate refining steps integrated in parallel in a pulp refinement stage.
- Lastly, according to another embodiment, varyingly modified fibrous raw materials result in a product according to the invention if these varyingly modified fibrous raw materials are used in combination, for instance in that this mixture, by being supplied to a specific channel of a multi-layer headbox during sheet making, leads to a layered intermediate product or, optionally after further processing, leads to a layered final product.

The present invention will now be explained in more detail by means of examples, without excluding other applications.

## EXAMPLES

### Test methods

The following test methods were used to evaluate the oxidized fibrous materials according to the invention as compared to fibrous materials which correspond, but which have not been modified by oxidation.

#### 1) Producing the test sheets

The test sheets (having a basis weight of approx. 80 g/m<sup>2</sup>) were made in accordance with the Rapid Köthen method (DIN 54 358-1, February 1981; see also ISO 5269-2: 1980). Before being tested in terms of physical properties e.g. by means of the tensile test, the thus obtained test sheets were always conditioned for a duration of at least 12 hours in a standard climate at a temperature of (23±1) °C and a relative humidity of (50±2) % in accordance with DIN EN 20187, Paper, Cardboard and Pulp, a standard climate for pretreatment and testing and a method of monitoring the climate and pretreatment of samples, November 1993 (see ISO 187 : 1990).

#### 2) Initial wet strength (width-related breaking strength (wet)) and tear length (wet)

The wet strength according to DIN ISO 3781, Paper and Cardboard, tensile test, determination of the width-related breaking strength after immersion in water, October 1994 (identical to ISO 3781 : 1983), is herewith defined as initial wet strength of the fibrous material networks according to the invention, e.g. paper/tissue paper/nonwoven.

When experimentally checking the invention, the tensile test was accordingly performed by means of an electronic tensile test apparatus (Model 1122, Instron Corp., Canton, Mass., USA)

with a constant rate of elongation of 10 mm/min using a Finch device. The width of the test strips was 15 mm. The strip length was about 180 mm. The free clamping length when using the Finch clamp was about 80 mm. The test strip was secured with both ends in a clamp of the test apparatus. The other end (loop) formed in this way was placed around a pin and treated at 20°C with distilled water until complete saturation. The soaking period of the samples before tensile testing was fixed at 30 s. Six test strips at a time were measured, the result being indicated as an arithmetic mean.

To ensure that the wet strength of the samples has fully developed, which is particularly necessary in the case of samples in which additional wet-strength agents were used to boost wet strength, e.g. by their addition in the mass, the samples to be tested were always artificially aged before conducting the tensile test. Aging was effected by heating the samples in an air-circulating drying cabinet to  $(125 \pm 1) ^\circ\text{C}$  for a period of 10 min.

A similar approach applies to paper/tissue paper/nonwoven products, modified only to the extent that the test strips to be examined were taken from the finished product itself or from the product made thereof and that they do not originate from a laboratory test sheet.

As regards tissue paper and tissue products, DIN ISO 3781 is replaced by DIN EN 12625-5 Tissue Paper and Tissue Products - Part 5: determination of width-related wet load at break, January 1999. The strip width is then 50 mm, the free clamping length is shortened to about 50 mm, the depth of immersion of the loop formed by the test strip is at least 20 mm. The soaking duration (immersion time) is shortened to 15 s, the rate of elongation is set to a constant  $(50 \pm 2) \text{ mm/min}$ , the measurement of the breaking strength is performed on the sample immersed in distilled water.



Six test strips at a time were measured, the result being indicated as an arithmetic mean.

The tear length (wet) was calculated from the width-related breaking strength in accordance with the following formula (see TAPPI 494-96, Comment 9):

$$RL = 102000 (T/R)$$

where  $T$  is the initial wet strength in kN/m and  
 $R$  is the basis weight in g/m<sup>2</sup> (in a standard climate)

3) Dry strength (width-related breaking strength (dry)) and tear length (dry)

The dry strength was determined according to DIN EN ISO 1924-2, Paper and Cardboard, determination of properties under tensile load. Part 2: Method at a constant rate of elongation, April 1995, (ISO 1924-2 : 1994).

In the case of tissue paper and tissue products, the test is performed in accordance with DIN EN 12625 - 4, Tissue Paper and Tissue Products - Part 4: Determination of width-related breaking strength, elongation at break and tensile energy absorption, January 1999.

The tear length (dry) was calculated from the width-related breaking strength in accordance with the following formula (see TAPPI 494-96, Comment 9):

$$RL = 102000 (T/R)$$

where  $T$  is the tensile strength in kN/m and  
 $R$  is the basis weight in g/m<sup>2</sup> (in a normal climate)

#### 4) Relative wet strength

The relative wet strength (WS) was calculated as follows:

$$\text{rel. WS} = \text{BS}_{\text{wet}}/\text{BS}_{\text{dry}}$$

where  $\text{BS}_{\text{wet}}$  is the width-related breaking strength of the wet sample strip and  $\text{BS}_{\text{dry}}$  is the width-related breaking strength of the dry sample strip, and these values were ascertained in the manner described above.

#### 5) Determination of the carboxyl and aldehyde content

For the determination of the C(6)-carboxyl and/or -aldehyde contents in the cellulosic material of the invention, one of the following methods can be suitably adopted by a skilled person. In this context it should be noted that nitroxy-mediated, in particular TEMPO-mediated oxidations lead with a high selectivity to the oxidation of the C(6)-atom of the cellulosic glucose units to C(6)-aldehyde and/or C(6) carboxy groups. For this reason the methods 5.1. (conductometric) and 5.4. (hydroxylamine) can be applied which measure the total content of aldehyde and/or carboxy groups. The remaining methods 5.2. (uronic acid determination) and 5.3. (NMR) allow a specific distinction of C(6)-aldehyde and/or carboxy groups, even if other aldehyde and/or carboxy groups are present within the cellulose chain..

5.1.) The content of carboxyl groups in the fibers' cellulose chain can be detected by a conductometric titration and is calculated by converting the thus obtained charge value (into  $\mu\text{mol/g}$ ).

The aldehyde content is obtained by

- performing a first conductometric titration with the oxidized cellulose to determine the carboxyl group content,

- selectively oxidizing the aldehyde groups into carboxyl groups as described below
- performing a second conductometric titration to detect the content of additionally formed carboxyl groups and
- deducting the charge values obtained in the first and second conductometric titrations from one another and converting them into  $\mu\text{mol/g}$ .

The weight data (g) refer to the fibrous material dried for 6h at 105°C (oven-dried).

The conductometric titration was performed by titration with sodium hydroxide after lowering the pH of the fiber suspension (pulp density <1%) using HCl (pulp density <1%) to about 3. At pH 3, an ion exchange is produced at the carboxylate functions so that the H- form is obtained. An optimum NaCl concentration ( $0.2 \times 10^{-3}$  M) is used to suppress the Donnan equilibrium, i.e. to suppress the difference in pH between the fiber and the pH of the surrounding solution. During the titration, nitrogen gas is passed through the suspension to remove O<sub>2</sub> and CO<sub>2</sub> that disturb the titration. Both the changes in pH and the changes in conductivity are recorded during the titration. The length of the conductivity plateau is taken as a gauge for the amount of weak acids in the sample, and this plateau is calculated from the volume of sodium hydroxide solution in use and its concentration. The measuring method is performed at a temperature of 20°C.

A suitable method of performing the conductometric titration and determination of the COOH content is also described by S.Katz in "*Svensk Papperstidning*" 6/1984, p.48. S. Katz also describes the distinction between sulfonic acid groups and COOH groups in sulfite pulp.

The oxidation of the aldehyde groups into COOH groups was performed as follows. The pulp (1-2g) was suspended in deionized water (100ml) and the pH adjusted to 5 using

HCl/NaOH. Before oxidation, a stoichiometric amount of  $\text{H}_2\text{O}_2$  (relative to the estimated amount of aldehyde functions, see below) is added in order to suppress any formation of chlorine during the reaction: One mol of aldehyde groups requires the addition of 1 mol  $\text{NaClO}_2$ , so that the aldehyde content should be estimated at this time. The  $\text{NaClO}_2$  consumption can nevertheless be monitored and an excess (approx. 10%) used. For those skilled in the art the reaction can be followed by the pH drop. The  $\text{NaClO}_2$  is added in small portions while stirring the suspension, keeping the pH at 5 (temperature 20-25°C). After the addition of  $\text{NaClO}_2$ , sodium hydroxide is optionally used to re-adjust the pH to pH 5 and the suspension is left to agitate over night. After drainage, the pulp can be used, as described above, for the conductometric measurement of the COOH content.

5.2.) Another more selective method for determining the content of C(6)-aldehyde/carboxy groups in the fibrous material of the invention is the Blumenkrantz method (N. Blumenkrantz and G. Asboe-Hansen, Anal. Biochem. 1973, 54, 484). This method is based on the colorimetric determination of a pink compound arising when a decomposition product of the uronic acid polymer (C6-carboxy cellulose) reacts with 3-hydroxybiphenyl.

To a sample containing 1-20  $\mu\text{g}$  oxidized fibrous material (dissolved in 0,2 ml water) 1.2 ml of a solution of 0,0125 M boric acid (e.g. obtainable from E. Merck, Germany) in conc. sulfuric acid (95-97%; e.g. obtainable from E. Merck, Germany) is added. The sample is heated in boiling water for 5 minutes, followed by cooling in ice (to room temperature or below). Then 20  $\mu\text{l}$  of an aqueous solution of 0,2% 3-hydroxybiphenyl e.g. obtainable from Aldrich) is added. After 15 minutes incubation the extinction is measured ( $\lambda = 520\mu\text{m}$ ). D-glucuronic acid or its lactone (both e.g. obtainable from Aldrich) is used as reference material.

If the sample to be analysed turns out to be poorly soluble in water (generally at a low degree of oxidation), the above method is modified by dissolving the sample in 90% sulfuric acid/boric acid mixture obtained by adding 10 vol.% water to 90 vol.% of a solution of 750 mg boric acid in 11 conc. sulfuric acid (E. Merck, as above). From this sulfuric acid/boric acid solution of the fibrous material 0.2 ml are taken and added to 0.2 ml water. To this mixture 1.0 ml of a solution of 0.0125 M boric acid in conc. sulfuric acid (E. Merck, as above) is added. Then the procedure is continued as above. ). Also in this case D-glucuronic acid or its lactone (both e.g. obtainable from Aldrich) is used as reference material.

The aldehyde content can be determined, by

- Determining the content of uronic acid groups before and after the oxidation of C(6)-aldehyde groups to C(6)-carboxy groups (uronic acids) with chlorite and hydrogen peroxide, and
- Subtracting these values.

5.3.) An alternative for the determination of C(6)-aldehyde contents involves the conversion of the oxidized material with hydroxylamine hydrochloride to the oxim. The C(6)oxim displays a distinct signal in  $^{13}\text{C}$  NMR spectra.

5.4.) A further option for determining the aldehyde content involves the hydroxylamine method:  
to a sample of 25 ml water containing 1g of aldehyde-containing fibres, 0.20 g hydroxylammonium chloride (e.g. obtainable from E. Merck, Germany) was added which results in a gradual decrease of the pH value. The reaction mixture is heated for at least 3 hours at 40 °C. The amount of HCl released was then titrated with 0.1 M NaOH (Titrisol, obtainable from Merck, Germany) up to end point of pH 3,4 and the consumed NaOH recalculated to  $\mu\text{mol}$  aldehyde/g fibres.

6) WRV (water retention value)

The WRV is determined in the following way.

The principle of determining the WRV is based on centrifuging swollen pulp samples at room temperature in a special-purpose centrifuge beaker with 3000-fold gravitational acceleration. The WRV in percent (mass portions in percent) indicates the portion of water in the sample that cannot be centrifuged.

Implementation conformed with German *Zellcheming* Code of Practice IV/33/57 (issued on January 1, 1957)

- A fibrous material treated with excess water as a swelling agent is taken.
- The tubes for the centrifuge inserts are filled to about 2/3 of the volume with the moist pulp sample without pressing firmly.
- A triple determination is to be performed each time.
- The tubes are inserted into the centrifuge beaker.
- Centrifuging conditions: 15 min at 4800 rpm
- After the centrifuge comes to a standstill, the tubes are taken out and the centrifuged substance immediately transferred with the aid of pincers as completely as possible into the weighing bottles previously dried at 103°C and tared at room temperature where they are weighed (remove glass spheres beforehand)
- The samples are now dried for at least 6 hours in the circulating-air drying cabinet, immediately seal when taking them out and allow them to cool in the desiccator. Now reweigh.

The calculation is made on the basis of the following equation:

$$WRV = \frac{(W-D)}{D} \times 100$$

where W = the weight of the moist substance, D represents the dry weight of the substance; and W minus D = the weight of the absorbed water.

#### 7) Other parameters

Other test methods were performed in accordance with German DIN standards or in conformity therewith. In those cases in which there was deviation from the standardized test method, this is described.

DIN EN 20638	Pulp: determination of the dry-solids content (ISO 638: 1978); German version EN 20638:1993
DIN EN 25264-3	Pulp: laboratory beating - Part 3: Jokro mill method (ISO 5264-3 1979) German version EN 25264-3: 1994
DIN EN 25651	Paper, cardboard and pulps: measurement units for designation of properties (ISO 5651:1989); German version EN 25651:1993
DIN ISO 5267-1	Chemical pulp and mechanical pulp; examination of the dehydration behavior; Schopper-Riegler method; identical to ISO 5267-1: 1979
DIN 54357	Examination of pulp, determination of the kappa number

Example 1:

50g of a bleached softwood kraft pulp (Grapho Celeste, SCA Östrand Mill, Sweden) was swollen for 24h in deionized water. The pulp was then beaten in a disintegrator and a consistency of 1.5 %, relative to the dry weight (oven-dried) of the fibers was set. The pH was set to a pH of 3.5 by addition of 55 ml 2n hydrochloric acid (HCl).

A 13% aqueous 4-hydroxy TEMPO solution corresponding to the amounts (ml) indicated in Table 3 was then added to the pulp suspension and stirred constantly. The wt.% data refer to the dry weight of the fibers (oven-dried). After 5 min, sodium hypochlorite was added and stirred vigorously. The reaction time given in Table 1 refers to the period from the addition of NaOCl.

At the end of the reaction, the pulp was washed with tap water on a Büchner funnel in a ratio of 1:10. Standardized test sheets were then made from the thus treated pulp, as explained above, and the strength properties were determined on the basis of these sheets.

The reaction conditions and strength properties are summarized in Tables 1 and 2. "No. 0" stands for a reference sample of an unoxidized bleached softwood kraft pulp (Grapho Celeste, SCA Östrand Mill, Sweden).



Table 1: Reaction conditions (BSWK)

No.	Time	4-hydroxy TEMPO			NaOCl		2n HCl	
		[wt%]	[g]	10g/l sol.	[%]	[13 wt.%]		
				[ml]		[ml]	[wt%]	[ml]
No. 1	1h	1.0	0.5	50	5.0	19	4.0	55
No. 2	1h	2.0	1.0	100	5.0	19	4.0	55
No. 3	3h	2.0	1.0	100	5.0	19	4.0	55

Table 2: Fibrous material properties of the not beaten pulp and of the modified pulp (BSWK) beaten for 5 min

	Tear length dry not beaten	Tear length wet not beaten	rel. wet tear len.	Tear length dry beaten for 5'	Tear length wet beaten for 5'	rel. wet tear len.	WRV not beaten
	[m]	[m]	[%]	[m]	[m]	[%]	[%]
No. 0	3417	19	0.6	5945	20	0.3	99.2
No. 1	3071	236	7.7	5152	280	5.4	98.6
No. 2	3232	423	13.1	4279	564	13.2	101.7
No. 3	3217	411	12.8	5557	511	9.2	98.6

The results show that a significant increase in wet strength was achieved by introducing aldehyde and/or carboxy groups into the cellulose chains of the pulp, without causing any variation in the WRV. This entails the advantage that e.g. the pulp's drainability is not affected during the production of the nonwoven or paper product and hence an increased energy expenditure is unnecessary to dry the paper or nonwoven.

Example 2:

A bleached hardwood sulfite pulp was treated under acidic pH conditions with 4-hydroxy TEMPO using NaOCl as a primary oxidizing agent. The conditions are listed in Table 3.

16g (relative to oven-dried fibrous material) was then used to produce test sheets (basis weight of 80g/m<sup>2</sup>) whose physical properties were analyzed as described above.

The properties of the hardwood sulfite pulp treated with 4-OH TEMPO are listed in Table 4.

Table 3: Conditions for treating a hardwood pulp

No.	Time	4-OH TEMPO	NaClO [13%]	HCl [2n]	pH
	[min]	[g/50g oven-dried fibrous material]	[%]	[ml]	[-]
4	60	0.75	5	10	3.3
5	60	1.00	5	10	3.3
6	180	0.50	5	10	3.3
7	180	0.75	5	10	3.3
8	180	1.00	5	10	3.3

Table 4: Strength properties of the hardwood sulfite pulp  
treated with 4-OH TEMPO  
(test sheet properties)

Test	Sheet weight	Basis weight	Breaking strength dry	Tear length dry	Breaking strength wet	Tear length wet	rel. wet strength
[No.]	[g]	[g/m <sup>2</sup> ]	[N/15mm]	[m]	[N/15mm]	[m]	[%]
Ref.	3.04	95.82	18.48	1285.7	0.151	10.5	0.8
4	2.53	79.82	27.19	2270.9	4.602	384.4	16.9
5	2.56	80.60	23.94	1980.1	4.687	387.7	19.6
6	2.60	81.85	29.38	2393.0	3.379	275.2	11.5
7	2.55	80.39	26.53	2200.1	4.127	342.2	15.6
8	2.32	73.04	24.70	2254.5	3.974	362.7	16.1

It was surprisingly found that a relative wet strength of almost 20% can be achieved. At the same time, however, it is also shown that the breaking strength (dry) of the pulps treated with TEMPO and oxidizing agent is much higher than the untreated pulp, thus making it possible to improve clearly not only the wet strength, but also the dry strength.

#### Example 3:

Various additives that act as wet-strength agents were added to a blend of two modified fibrous materials.

The modification occurred in the following way:

64g pulp was suspended in water at a consistency of 1.5%. An acidic pH of 2.5 was set by addition of 2n HCl and 2 wt.%, relative to oven-dried fibrous material, of 4-OH TEMPO was added and stirred constantly. 25 ml of a 13% sodium

hypochlorite solution was then added to the acidic suspension of fibrous material and left to react at room temperature for 90 min. The pulp was then washed with deionized water and a ratio of 30% hardwood sulfite pulp and 70% BSWK was set. The corresponding amounts of wet-strength agents Kymene and CMC (carboxymethylcellulose) were then added.

The amounts of added wet-strength agent (WSA) are listed in Table 5.

Table 5: Fibrous material properties of the modified pulp blend (30% hardwood sulfite pulp and 70% BSWK)

No.	Breaking strength dry [N/15mm]	Tear length dry [m]	Breaking strength wet [N/15mm]	Tear length wet [m]	Rel. wet strength [%]
9	30% Excellent + 70% Celeste, beaten [22°SR]				
	Reference				
	69.92	6069.4	12.67	1099.8	18.1
10	30% Excellent + 70% Celeste, beaten [22°SR]				
	10 kg/t WSA [Kymene]				
	78.13	6798.1	28.66	2493.7	36.7
11	30% Excellent + 70% Celeste, beaten [22°SR]				
	5 kg/t CMC + 10 kg/t WSA [Kymene]				
	87.80	7493.7	33.38	2849.0	38.0

#### Example 4

A pre-dried bleached (TCF) kraft pulp (Grapho Celeste) from the SCA pulp mill at Östrand was beaten in a disintegrator, then drained and stored in the refrigerator until oxidation.

An aqueous suspension was produced from the thus treated pulp. The pH of the suspension was set to 8.5-9.3 by means of an aqueous  $\text{NaHCO}_3/\text{Na}_2\text{CO}_3$  buffer. First 6mg TEMPO per g fiber (oven-dried), then 0.86 mmol NaOCl per g fiber (oven-dried) were added as primary oxidizing agents to this fiber suspension at a temperature of 40°. The reaction duration (time from start of NaOCl addition) is indicated in Table 9 below.

The thus obtained fibers were filtered off and washed with water.

To produce the test sheets, the oxidized fibers were each put in 2l water in 30g portions. If necessary, the pH of the thus obtained suspension was adjusted using NaOH or HCl. Test sheets were then made and they were evaluated in accordance with the aforementioned measuring methods with regard to their WRV, their tensile strength index in the dry and wet states and their relative wet strength.

Table 6: Wet and dry strength properties of TEMPO-oxidized sulfate pulp

Oxidation time	WRV	Tensile strength index dry	Tensile strength index wet	relative wet strength
(hours)	[%]	[kNm/kg]	[kNm/kg]	[%]
0	106.0	28.1	0.0	0.0
3	115.5	6.8	3.3	12.2
4	117.5	27.5	4.1	14.8
5	119.5	24.4	3.3	13.4
6	120.0	26.1	3.3	12.6
8	122.5	26.9	3.2	12.0
11	122.0	27.9	3.0	10.7

The results show that the introduction of oxidized groups (primarily aldehyde here) into the pulp's cellulose leads to an increase in the strength of a paper made thereof.

#### Example 5

A sulfite pulp that had never been dried after production was beaten directly from pulp production in the still moist state in a pulp mill for 0, 5, 15 and 30 min.

The not beaten and beaten pulps were then oxidized in the same way as described in Example 4. The reaction duration was 3h or 6h.

The reference samples "NaOCl Ref." of Table 7 were treated under the same conditions as described above, though only with sodium hypochlorite and buffer (without TEMPO). The reference samples "Ox-Ref" of Table 7 were treated under the same conditions as described above, though only with buffer.

Test sheets were then made in the same way as in Example 4 and evaluated. The results are shown in Table 7.

Table 7: Relative wet strength of TEMPO-oxidized sulfite pulp

			Tensile strength (wet)	Breaking length (wet)	Breaking length (dry)	relative wet strength
			[N/15mm]	[m]	[m]	[%]
NaOCl Ref.	Pulp 1	0'	0.66	56.1	3149.0	1.8
NaOCl Ref.	Pulp 1	5'	1.28	108.7	6143.0	1.8
NaOCl Ref.	Pulp 1	15'	1.66	141.0	7966.0	1.8
NaOCl Ref.	Pulp 1	30'	2.22	188.6	8508.0	2.2
Ox Ref.	Pulp 2	0'	0.39	33.1	3123.0	1.1
Ox Ref.	Pulp 2	5'	0.61	51.8	6602.0	0.8
Ox Ref.	Pulp 2	15'	0.71	60.3	8081.0	0.7
Ox Ref.	Pulp 2	30'	1.15	97.7	8689.0	1.1
Oxide 6h	Pulp 3	0'	13.79	1171.4	4097.0	28.6
Oxide 6h	Pulp 3	5'	26.61	2260.4	7157.0	31.6
Oxide 6h	Pulp 3	15'	30.69	2607.0	8628.0	30.2
Oxide 6h	Pulp 3	30'	30.42	2584.1	10385.0	24.9
Oxide 3h	Pulp 4	0'	16.06	1364.3	4080.0	33.4
Oxide 3h	Pulp 4	5'	37.95	3223.8	7828.0	41.2
Oxide 3h	Pulp 4	15'	36.93	3137.1	8543.0	36.7
Oxide 3h	Pulp 4	30'	50.62	4300.0	9159.0	46.9

The tensile strength index indicates the tensile strength in N/m divided by the basis weight (see TAPPI, T494-96, Definitions 2.5).

Conductometric measurements of different batches of the same type of pulp (sulfite pulp) subjected to the TEMPO-mediated oxidation used in this example (cf. conditions of example 4) over 3h and 6h, respectively, showed that the contents of introduced carboxy or aldehyde groups after 3 h were 20  $\mu\text{mol}$  COOH /g oven-dried fibers and 288  $\mu\text{mol}$  aldehyde/g oven-dried fibers. After 6h a second measurement indicated a considerably reduced amount of aldehyde groups and a corresponding increase

in total introduced COOH groups, which can be explained by the oxidation of C(6)-aldehyde to C(6)-carboxy groups. These results demonstrate the effects of the presence of C(6)-aldehydes on the wet strength properties of (tissue) paper, since the observed maximum of wet tensile strength and relative wet strength after 3h coincides with a high aldehyde content.

In addition, the results show that the strength achieved by the introduction of oxidized groups can be even further increased by beating the pulp used.

#### Example 6

2t air-dried standard Grapho Celeste (SCA Östrand Mill, Sweden) long-fibered kraft pulp with a consistency of 1.2% was suspended in the machine chests of a pulp-drainage machine. For this purpose, the pulp was dissolved by means of the pulper in the pulp-drainage machine. Fresh water (spring water) was used to dissolve the pulp, set the necessary pulp densities, and wash the treated, oxidized pulp. A pH of approx. 4.5 was set by addition of sulfuric acid. The pulp suspension also contained about 6wt.% of a wet strength agent (polyamide amine epichlorhydrine resin; Kymene SLX from Hercules), based on the weight of the oven-dried pulp. To blend the suspension, the acidically adjusted pulp suspension was continuously pumped and returned from one machine chest into a second machine chest. Both machine chests have an overflow into the other machine chest, thereby ensuring intimate blending.

1.5% 4-OH TEMPO relative to oven-dried fibrous materials was dissolved in the acidically adjusted pulp suspension. After complete blending, 5% NaOCl - relative to the oven-dried fibrous material - was added batchwise and reacted at 40°C with the 4-OH TEMPO. After a period of treatment of 2 hours,



the thus treated pulp was drained on the pulp-drainage machine and washed with fresh water at the end of the drain screen via the so-called hot-water channel. The pulp was then moved over the couch to the third press from where it is re-dissolved in the machine pulper and then, after further dilution of the pulp suspension in the machine chests to approx. 1.2%, re-drained on the pulp-drainage machine, pressed out via the first and second presses and then temporarily stacked as a moist web without further drying at a consistency of 30% pulp density.

Differing from the above-described technique, a bleached hardwood sulfite pulp (Excellent, Mannheim quality) was transferred in an aqueous suspension to the machine chest of the drainage machine. All other treatment steps corresponded to those described above.

Measurements of the contents of C(6) aldehyde and/or carboxy contents in the cellulosic fibers according to the Blumenkrantz method led to the following results:

- Sulfite pulp (Mannheim, Excellent): 65 $\mu$ mol aldehyde/g oven-dried fibers, 250 $\mu$ mol carboxy/g oven-dried fibers
- Kraft pulp (Östrand, Celeste): 63 $\mu$ mol aldehyde/g oven-dried fibers, 260 $\mu$ mol carboxy/g oven-dried fibers

Further processing of the thus treated pulp into a TAD raw tissue paper came about on the TAD pilot plant operated by the Valmet company (Karlstad, Sweden). In the test, the TAD raw tissue paper was produced from a pulp blend of the two aforementioned pulps in two versions, on the one hand from the non-oxidized pulps and on the other from the oxidized pulps. For this purpose, the pulp was dissolved in a pulper and adjusted with fresh water in a machine chest at a consistency of approx. 3%. In accordance with the conditions of the reference test in which a conventional untreated "Grapho Celeste" (kraft pulp, SCA Östrand mill) or sulfite pulp

("Excellent", SCA Mannheim mill) was used, a TAD raw tissue was made from a pulp ratio of 30% oxidized sulfite pulp to 70% oxidized Grapho Celeste kraft pulp. All the other production conditions were kept the same.

The strength values are shown in the attached table. The strength values refer to a one-ply tissue paper which was measured in the aforementioned measuring method by forming a loop around the pin of a tensile test device.

Table 8: strength values of tissue paper

Base tissue	Dry breaking strength, in transverse direction [N/50 mm]	Wet breaking strength, in transverse direction [N/50 mm]	Relative wet strength [%]
Pulp oxidized with 4-OH TEMPO	20.1	7.9	40
Reference pulp	17.9	5.5	31

Example 7: Production of 6-aldehyde cellulose

One gram of oven-dried totally chlorine-free bleached and sheet-dried Kraft pulp fibers (SCA Östrand mill, Grapho Celeste) was suspended in 100 ml of water. To this suspension 18 mg of TEMPO (0.1 mmol) and 9 mg of peroxidase (HRPO), type VI (290 units/mg) were added. The pH was adjusted to 5.1 with aqueous acetic acid (0.1 M). A hydrogen peroxide solution (1.5 ml 30% in 50 ml) was added stepwise, (30-50 µl every 2 minutes) for 8 hours. After peroxide addition the pH decreased, but it returned to its original value (5.5) after a

few moments; therefore, no pH adjustment was necessary during the reaction. After 21 h a sample was analysed by addition of hydroxylammonium chloride. According to this hydroxylamine method, the sample contained 26% (260mg) of C6-aldehyde cellulose. Based on a molecular weight of  $M = 160 \text{ g/mol}$  for the anhydroglucose unit, this corresponds to a content of  $1600 \mu\text{mol}$  C(6)-aldehyde per g oven-dried fibrous material.

## CLAIMS

1. A cellulose-containing fibrous material, wherein hydroxy groups were oxidized at the C(6) of glucose units of the cellulose into aldehyde and/or carboxy groups.
2. A cellulose-containing fibrous material according to claim 1, wherein the total content of aldehyde and/or carboxy groups is at least 50  $\mu\text{mol/g}$  fibrous material (as a dry content based on DIN EN 20638).
3. A cellulose-containing fibrous material according to one or more of claims 1-2, wherein the surfaces of the fibrous material used for oxidation are activated.
4. A paper or nonwoven comprising said cellulose-containing fibrous material according to one or more of claims 1-3.
5. A paper or nonwoven according to claim 4, wherein said paper or nonwoven is a tissue paper.
6. A paper or nonwoven according to claim 3 or 4, wherein said paper or nonwoven exhibits a relative wet strength of more than 10 %.
7. A paper or nonwoven product comprising at least one ply of said paper or nonwoven according to any of claims 4 to 6.
8. A paper or nonwoven product according to claim 7, wherein said paper or nonwoven product is a tissue product.
9. A tissue product according to claim 7 or 8, said tissue product having the form of a cleaning wipe, sanitary product, paper handkerchief, household towel, towel, cloth for facial use, napkin/serviette, bed linen or a garment.

10. A method of producing said cellulose-containing fibrous material according to one or more of claims 1-3, comprising the step of:
- oxidizing a cellulose-containing fibrous material using a nitroxy compound optionally in combination with a primary oxidizing agent.
11. A method according to claim 10, wherein the organic nitroxy compound is a sterically hindered, organic non-conjugated nitroxy compound.
12. A method according to claim 10 or 11, wherein said organic nitroxy compound is a 2,2,6,6-tetramethylpiperidiny1-1-oxyl (TEMPO) optionally substituted in 4 position.
13. A method according to any of claims 10 to 12, wherein said primary oxidizing agent is chosen from a hypohalite, ozone, a peracid, a metal-containing oxidizing agent and an oxidase.
14. A method according to any of claims 10-13, wherein peracid is used in the presence of a catalytic amount of halide at a pH of 5-11 for the purpose of oxidation.
15. A method according to any of claims 10-13, wherein oxidation is performed using hypohalite or ozone as a primary oxidizing agent and a 4-hydroxy, 4-amino or 4-amido substituted 2,2,6,6-tetramethylpiperidiny1-1-oxyl at a pH of 1-7.
16. A method according to any of claims 10-13, wherein oxidation is performed using MnO<sub>2</sub> as a primary oxidizing agent at a pH of 2-8.
17. A method according to claim 10, wherein oxidation is performed stoichiometrically using 4-acetamido-2,2,6,6-

tetramethylpiperidiny1-1-oxyl (4-acetamido TEMPO) at an acidic pH (<7).

18. A method according to any of claims 10-17, wherein the surfaces of the fibers in use are activated by mechanical treatment before oxidation.
19. A method of producing a paper or nonwoven, comprising the steps of
  - wet laying said oxidized cellulose-containing fibrous material of claims 1-3,
  - pressing the wet-laid fibrous material, and
  - drying the pressed fibrous material.
20. A method according to claim 19, wherein said paper is a tissue paper, and said method comprises a pre-drying step based on TAD technology and is followed by a creping step.
21. A method according to claim 19, wherein said paper is a tissue paper, and said method comprises a wet rush transfer step prior to the drying step..
22. A method according to any of claims 19 to 21, wherein said obtained paper, tissue or nonwoven is further processed into a paper, tissue or nonwoven product using at least one process step chosen from: cutting to size, producing a plurality of plies, producing mechanical ply adhesion, volumetric and structural embossing, application of adhesive, folding, imprinting, perforating, application of lotions, calendering, stacking, rolling up.

## INTERNATIONAL SEARCH REPORT

International Application No

PCT/EP 00/01538

## A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 C08B15/02 C08B15/04 D21H11/20

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 C08B D21B D21C D21H

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

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Y	column 1, line 4-8; claims 1,7,8,22; examples 1,5 -/-	9,11-18, 20,21

☒ Further documents are listed in the continuation of box C.☒ Patent family members are listed in annex.

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